

ARTIFICIAL RAINDROP ALGORITHM BASED CONTROL FOR FAULT TOLERANCE AND RECONFIGURATION OF DISTILLATION COLUMN

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Abstract: *In this paper, a novel nature-based meta-heuristic method, named artificial raindrop algorithm is proposed. This algorithm is stimulated from the phenomenon of natural rainfall and applied for nonlinear distillation column using parallel cascade control. Distillation column is an important process in chemical engineering. Distillation is a technique of separating mixtures with given contrasts in volatilities of components in a boiling fluid mixture. Cascade control scheme is efficient for systems that have large time constants and disturbances. It provides fast recovery from disturbances. Among the two methods of cascade such as series and parallel cascade, later reduces steady state error compared to series cascade. In this paper, various controllers such as PID and fuzzy gain scheduling PID controller are analyzed for flow control with fault tolerance in distillation column. Proposed artificial raindrop algorithm based results are compared with the PID and fuzzy gain scheduling PID controller based control to validate the enhanced performance of the proposed system. Entire system is analysed using Matlab/Simulink.*

Keywords: *Parallel Cascade Controller, Distillation Column, Fault Tolerance, PID, Fuzzy Gain Scheduling Controller, Artificial Raindrop Algorithm.*

1. Introduction

In a chemical and petrochemical industry, distillation plays vital role in separation[1-2]. Design and control of distillation systems are important in the aspect of security, pollution and cost reduction[3-5]. In this paper, wood and berry model of distillation column is considered for analysis because the model was established as a good, widely used during recent decades in many researches. Cascade control is extensively used in process industries to lower the effects of probable disturbances and to enhance the dynamic performance of the closed-loop system[6-10]. The cascade control structure consists of two loops: primary (outer) loop and secondary (inner) loop. Cascade control can be classified as series and parallel cascade control. Series cascade is applicable for the system where disturbance and the manipulated variable

affect the primary output through the secondary output[11]. Meanwhile, in distillation process the disturbance and manipulated variables concurrently influence primary and secondary outputs, parallel cascade control is proposed in this paper.

Luyben introduced parallel cascade control for distillation column with the comparative analysis of series cascade control[12]. From the analysis, it is noted that parallel cascade control reduces steady state error. PinakPani Biswas et al. (2009) analyzed nonlinear control of distillation column using feedback linearizing systems[13]. A simple nonlinear controller is analyzed by Chien et al. (1997) to control the product quality of distillation columns using model predictive control with disturbance rejection[14]. Daniele Semino and Alessandro Brambilla(1996)[8] analysed various possible Internal Model Control (IMC) structures for distillation control in series and parallel cascade control. The system is analysed for both in the nominal case and in the presence of uncertainties. Puneet Mishra et.al (2015) [15] analysed an intelligent control algorithm of Fractional Order Fuzzy PID controller for distillation control. Simulations results are validated with the comparative analysis of fuzzy PID controller. Lee et al. (2006) proposed an analytical method of PID controller design for parallel cascade control taking into account the interaction between primary and secondary control loops[16]. Conventional control techniques in distillation column control use model of the process which is highly nonlinear and complex. In this article, fuzzy gain scheduling (FGS) PID controller is applied in distillation column control which deals with unknown data.

Novel optimization method of Artificial Rain Drop (ARD) algorithm is proposed in this paper for flow control in distillation. The name of algorithm clearly states that it mimics the varying process of a raindrop, including the generation, descent, collision, flowing and the updating of a raindrop.

2. Parallel Cascade Controller On Distillation Column

Mathematical model of wood and berry distillation column is stated as follows.

$$\begin{bmatrix} X_D(S) \\ X_B(S) \end{bmatrix} = \begin{bmatrix} P_{11}(S) & P_{12}(S) \\ P_{21}(S) & P_{22}(S) \end{bmatrix} \begin{bmatrix} R(S) \\ S(S) \end{bmatrix}$$

Where,

X_D – Overhead product Composition

X_B – Bottom product Composition

P_{11} – Direct process transfer function, relating overhead composition to reflux flow

P_{12} – Interacting process transfer function, relating overhead composition to steam flow

P_{21} – Interacting process transfer function, relating overhead composition to steam flow

P_{22} – Direct process transfer function, relating bottoms composition to steam flow

R – Reflux flow rate

S – Steam flow rate

In a distillation column control of an overhead composition, cascaded onto the control of a tray temperature is a classic model of a parallel cascade control system [18-19]. In case of a cascade control, the reflux flow rate is assigned as manipulated variable and composition or feed flow is considered as disturbance (d). The control of the system decides the purity of the overhead product and tray temperature. Fig 1 shows the parallel cascade control structure in which G_{cp} and G_{cs} are the primary and the secondary controller.

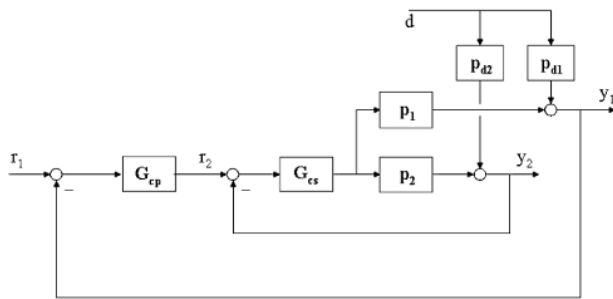


Fig.1. Parallel cascade control

In figure 1, p is the process transfer function, p_d is the process disturbance and G_c is the controller used in cascade control, where 1 and 2 stands for an outer and inner loop. Initially, the system is analyzed with conventional PID controller, then analyzed with FGS-PID and proposed ARD algorithm.

3. Fault Tolerance with Parallel Cascade Control

Fault tolerance is the major concern in the design of process control systems. In the absence of faults, a process will remain at the steady state, and the control is not necessary. Several control algorithms were proposed to improve fault tolerance capability. Two controllers can be designed separately for servo purposes and Fault Tolerance. This kind of approach raises the complication of control system design by designing two controllers for a single pair of input and output. Using the combination of primary and secondary measurements, a simpler approach can be taken to overcome the load fault problems. For this principle, the parallel cascade control structure is used, wherein the primary controller is intended for the servo purpose and the secondary controller is deliberate for the Fault tolerance. In the further analysis, fault is taken as a disturbance in a system. The major criteria for designing reconfiguration controller are its ability to sustain the acceptable performance even after fault. In this paper gain scheduling and optimization controllers are analysed.

Transfer function of the outer loop and inner loop of the system analyzed are given by [16]

$$P_1 = P_{d1} = \frac{e^{-4s}}{(20s + 1)} \quad (1)$$

$$P_2 = P_{d2} = \frac{1}{(10s + 1)} \quad (2)$$

P_1 and P_2 are the process transfer functions of outer and inner loop whereas P_{d1} and P_{d2} are disturbance transfer function of the outer loop and inner loop. Simulation analyses are done using Matlab/Simulink and the simulation model is shown in figure 2.

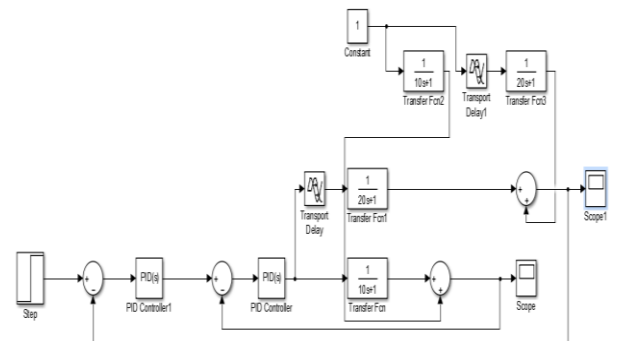


Fig.2. Simulink model of parallel cascade control

4. PID Controller in Distillation

A Proportional–Integral–Derivative controller (PID controller) is a conventional controller widely used in many industries for its simple control[19-21]. In this paper Ziegler Nichols method of tuning is used. The Ziegler–Nichols tuning method is a heuristic method of tuning a PID controller. This tuning rule is meant to give PID loops abest disturbance rejection.The transfer function of a standard PID [22-23] controller in an ideal form is

$$G(s) = K_p + K_i \left(\frac{1}{s}\right) + K_d s \quad (3)$$

Where K_p , K_i and K_d are the proportional, integral and derivative gain respectively. Each gain has different effect on the speed of response and stability. Two PID controllers are proposed in the parallel cascade controlto control flow and temperature. Both PID controllers are tuned using Ziegler Nichols method of tuning.

5. Fuzzy Gain Scheduling PID In Distillation

Fuzzy gain scheduling PID is a method of online tuning of gains of PID controller based on control parameters[24-26]. Fixed value of PID controller gains irrespective of change in input oscillates and delays the settling of output [27-30]. Hence in this analysis fuzzy logic controller is proposed to tune the gains of PID controller. In the case of distillation cascade control, it receives flow error as input to produce K_p , K_i and K_d as output. In this analysis, FGS PID controller is applied in outer loop and PID controller is applied in inner loop.

In this paper, Mamdani type of fuzzy with the min-max method of fuzzification is used. Centroid method of defuzzification is applied to attain output[31]. Block diagram of FGS PID for distillation control is shown in figure 3.

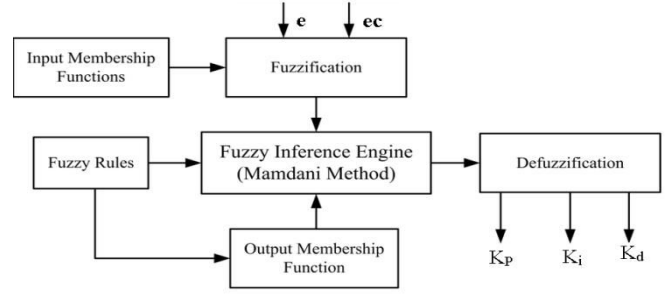


Fig.3. Block diagram of FGS PID

Rules in the FGS PID controller decides the output based on input whereas the number of rules in controller decides the processing time in real time implementation. In this paper, 25 rules are applied after many analyses. Flow error (e) and change in error (ce) are inputs of controller with the membership functions of Positive High, Positive low, zero, Negative low and negative high are stated as {PH,PL, Z, NL,NH}. K_p , K_i and K_d are outputs with the membership functions of {Z, S, M, B}. Simulation model of FGS-PID is shown in figure 4.

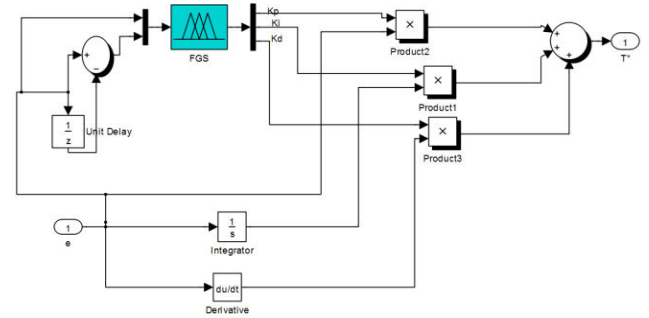


Fig.4. Simulation model of FGS-PID

From the figure 4 model, it is noted that flow controller output (T^*) of FGS-PID is a reference for temperature controller (inner loop).

Figure 5 shows the membership function of inputs e and ce. Figure 6 (a), (b), (c) shows the membership functions of outputs.

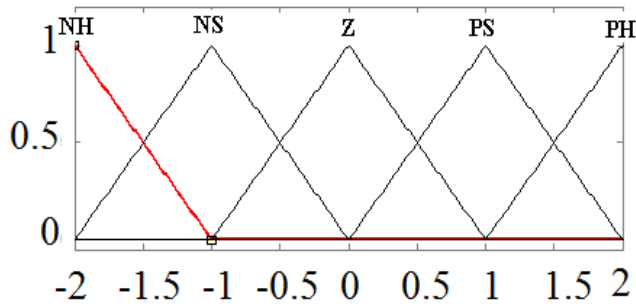


Fig.5. Membership functions of inputs e and ce

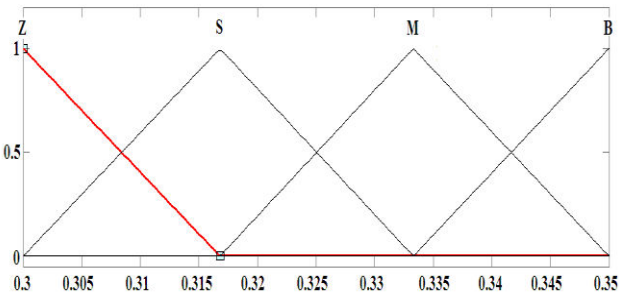


Fig.6a. Fuzzy membership functions of output k_p

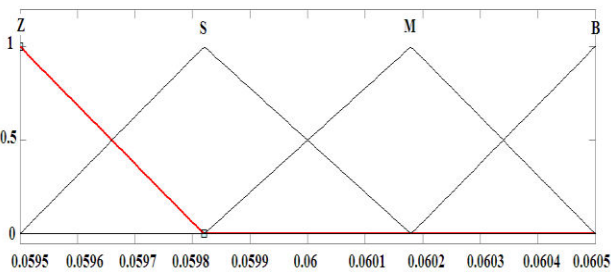


Fig.6b. Fuzzy membership functions of output k_i

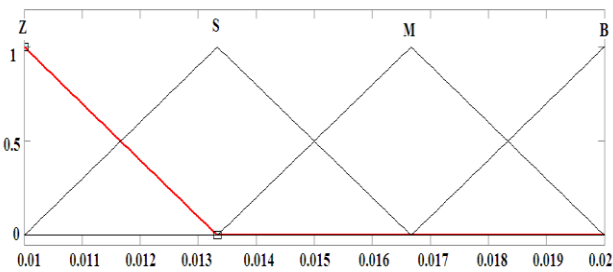


Fig.6c. Fuzzy membership functions of output k_d

The rules are framed such as

If (E is PH) and (EC is PH) then (K_p is B) (K_i is B) (K_d is Z)

If (E is Z) and (EC is Z) then (K_p is Z) (K_i is Z) (K_d is Z)

If (E is NH) and (EC is PH) then (K_p is M) (K_i is Z) (K_d is Z)

Similarly based on the value of present error and change in error K_p , K_i and K_d are tuned. The table 1, 2, 3 shows the rules for K_p , K_i and K_d .

Table 1 Rules for K_p

ece	NH	NL	Z	PL	PH
NH	B	B	B	B	M
NS	M	B	S	S	S
Z	M	B	Z	S	B
PL	S	S	S	S	S
PH	M	B	B	M	B

Table 2 Rules for K_i

ec	NH	NL	Z	PL	PH
e					
NH	Z	Z	Z	Z	Z
NL	M	M	M	M	M
Z	B	B	Z	B	B
PL	S	M	M	M	M
PH	Z	S	B	B	B

Table 3 Rules for K_d

Fuzzy Gain Scheduling controller reduces the overshoot and steady state error, even though the overshoot and steady state error are to be reduced further.

6. Artificial Raindrop Algorithm

From the name of artificial raindrop algorithm, it is clear that it is the inspiration of principle of natural raindrops. This algorithm begins with vapors as initial population. Then, an individual altitude is considered as the individual fitness value. Due to the action of gravity from high altitude, the small raindrops will flow to low altitude direction. At last most of the small raindrops will stay in the location of the optimal solution. The five correspondences of ARD algorithm are discussed below.

Raindrop generation operator: In this step, by absorbing ambient water vapour in nature, the raindrop is generated. The position of the raindrop is assumed that it is the geometric centre of ambient water vapour. At each generation t , the raindrop generation operator φ_R^G on vapour population.

$$\text{Pop}(t) = \{\text{Vapor}_1(t), \text{Vapor}_2(t), \dots, \text{Vapor}_N(t)\} \quad (4)$$

is carried out as follows.

Define

ec e	NH	NL	Z	PS	PH
NH	Z	M	B	M	Z
NL	S	M	B	B	S
Z	S	B	B	M	Z
PL	S	B	M	M	S
PH	Z	S	M	S	Z

Raindrop

= {Vapor

$$= \left\{ \frac{1}{N} \sum_{i=1}^N \right.$$

Where N is the number of

population size.

Raindrop descent operator: By the action of gravity the raindrop straight drops from the cloud to the ground in the absence of effect of wind. This is equivalent to a disturbance in an evolutionary algorithm or one-dimensional mutation operator.

Hence, the raindrop descent operator φ_R^D on raindrop is executed as follows.

$$\text{New_Raindrop}(t) = \varphi_R^G(\text{Pop}(t)) \quad (6)$$

i.e.

$$\text{New_Raindrop}_{r_1}(t) = \text{New_Raindrop}_{r_2}(t) + \phi \cdot (\text{New_Raindrop}_{r_1}(t) - \text{New_Raindrop}_{r_2}(t))$$

where $r_1, r_2, r_3, r_4 \in \{1, 2, \dots, D\}$ are randomly chosen indexes, j is the corresponding index of decision variable in New Raindrop, and ϕ is a random number in the range (-1, 1).

Raindrop collision operator: In order to keep the population scale stability, number of small raindrops produced from the main drop when contacts with the ground are equal to the population size.

$$\text{Small_Raindrop}(t) = \varphi_R^C(\text{New_Raindrop}(t) \cup \text{Pop}(t))$$

i.e.

$$\text{Small_Raindrop}_{ij}(t) = \text{New_Raindrop}_j(t) + \text{sign}(\alpha_j - 0.5) \cdot \beta_j$$

Where i ($i = 1, 2, \dots, N$) and j ($j = 1, 2, \dots, D$) are the index of i th and the corresponding dimension of small raindrop, respectively. $k_2 f_1, 2, Ng$ is randomly chosen index, α_j and β_j are two uniformly distributed random

numbers in the range (0, 1) and $sign()$ stands for sign function.

Raindrop flowing operator: Due to the action of gravity, finally most of the small raindrops will stay in the locations with a relatively low elevation. Raindrop pool (RP) which comprises archives optimal solutions. The raindrop flowing operator φ_R^F on small raindrops is generated as follows.

$$\text{New_Small_Raindrop}(t) = \varphi_R^F(\text{Small_Raindrop}(t)) \quad (10)$$

i.e.

$$\text{New_Small_Raindrop}_i(t) = \text{Small_Raindrop}_i(t) + d(t - \lambda).$$

Where

$$d(t - \lambda) = \tau_1 \cdot \text{rand}_1 \cdot \text{sign} \left(F(\text{RP}_{k_1}) - F(\text{Small_Raindrop}_i) \right) + \tau_2 \cdot \text{rand}_2 \cdot \text{sign} \left(F(\text{RP}_{k_2}) - F(\text{Small_Raindrop}_i) \right)$$

where, in raindrop pool RP, RP_{k_1} and RP_{k_2} are any two of candidate solutions, rand_1 and rand_2 are two uniformly distributed random numbers in the range (0, 1), τ_1 and τ_2 are two step parameters of Small Raindrop flowing, $F()$ is the fitness function, $sign()$ stands for sign function, λ is a damping coefficient and can be chosen by the tournament selection procedure. However, each raindrop could not have been in the flowing in a real environment. They will stay in the locations with a relatively lower elevation or evaporate after numerous flowing. It is essential to commence a parameter *Max Flow Number* to manage the maximum number of flowing.

Raindrop updating operator: By the evaporation, the water vapor produced in the land water cycle system is mainly from surface water. In order to enhance the convergence rate and computational performance for global optimization problem, the raindrop updating operator φ_R^U is executed as follows.

$$\text{Pop}(t + 1) = \varphi_R^U(\text{Pop}(t) \cup \text{Small_Raindrop}(t)) \quad (13)$$

That is to say; a sort method is used to select the N best individuals as the next population from the above two populations. In this paper, a bubble-sort procedure is applied for ranking method.

The flow chart of artificial raindrop algorithm is shown in figure 7.

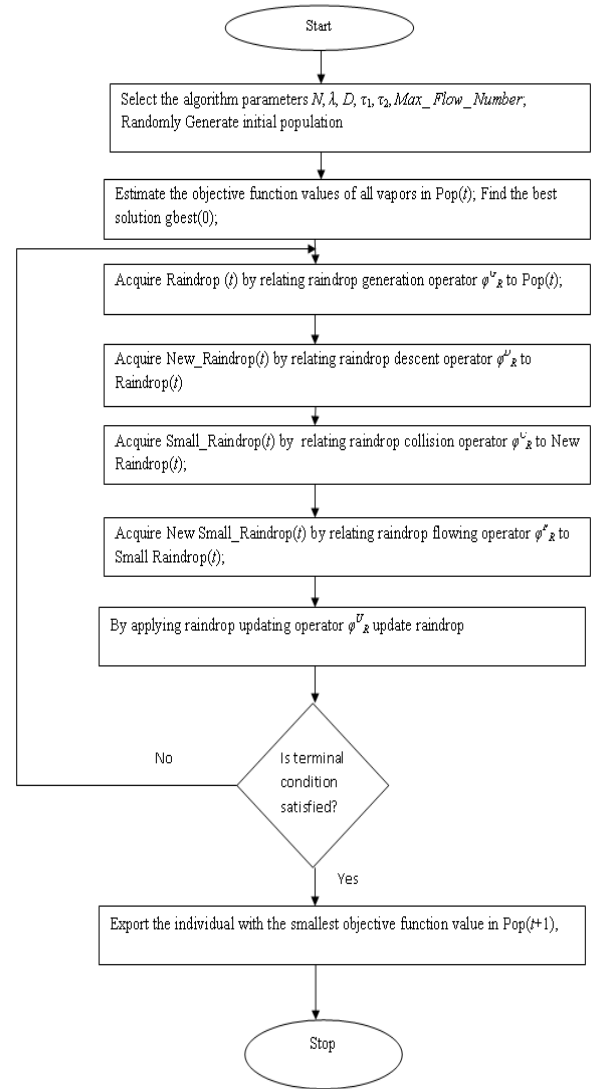


Fig.7.TheFlowchart of ARD

From the figure 7 steps of ARD algorithm is noted and described as procedure as follows.

6.1. Procedure of artificial raindrop algorithm

Procedure of artificial raindrop algorithm is stated in 8 steps as follows,

Step1. Initialization: Select the algorithm parameters N , λ , D , τ_1 , τ_2 , Max_Flow_Number ; Randomly Generate initial population $\text{Pop}(0)$; Set $t = 0$.

Step2. Evaluation: Estimate the objective function values of all vapors in $\text{Pop}(t)$; Find the best solution $\text{gbest}(0)$; $\text{RP}(0) = \text{gbest}(0)$;

Step3. Raindrop Generation: Acquire Raindrop (t) by relating raindrop generation operator ϕ_R^G to Pop(t);

Step4. Raindrop Descent: Acquire New_Raindrop(t) by relating raindrop descent operator ϕ_R^D to Raindrop(t);

Step5. Raindrop Collision: Acquire Small_Raindrop(t) by relating raindrop collision operator ϕ_R^C to New Raindrop(t);

Step6. Raindrop Flowing: Acquire New Small_Raindrop(t) by relating raindrop flowing operator ϕ_R^F to Small Raindrop(t);

Step7. Raindrop Updating: Acquire Pop($t+1$) by applying raindrop updating operator ϕ_R^U to Pop(t) U Small_Raindrop(t and update Raindrop) pool RP($t+1$);

Step8. Termination Test: If termination condition is satisfied, export the individual with the smallest objective function value in Pop($t+1$), stop the algorithm; otherwise, $t = t + 1$, go to Step 3.

6.2. ARD algorithm in distillation

In a distillation column control, ARD algorithm is applied to tune the gains of PID controller in an outer loop of cascade control. K_p , K_i and K_d are the output of ARD algorithm. $K_p=0.312$, $K_i=0.069$ and $K_d=0.011$ are the outputs ARD algorithm.

7. Simulation Results And Discussion

In a parallel cascade distillation set point of flow is set externally and is controlled by PID/ FGS PID/ARD algorithm. Output of flow controller is act as a setpoint to the temperature controller. It is controlled using PID controller. For an analysis, flow is set in the range of 40 to 100 which is act as a reference value for temperature control. Figure 8 to 10 shows the performance flow using various controllers such as by PID, FGS PID and ARD algorithm.

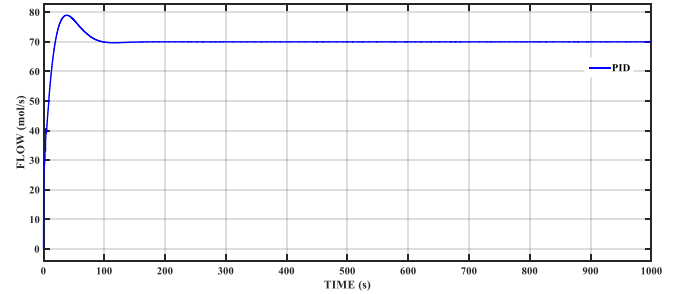


Fig.8. Flow performance of PID-based parallel cascade control at 70mols/s

From the figure 8, it is noted that flow sets in its reference value of 70 after peak overshoot of 11.43%, which is very high and to be reduced.

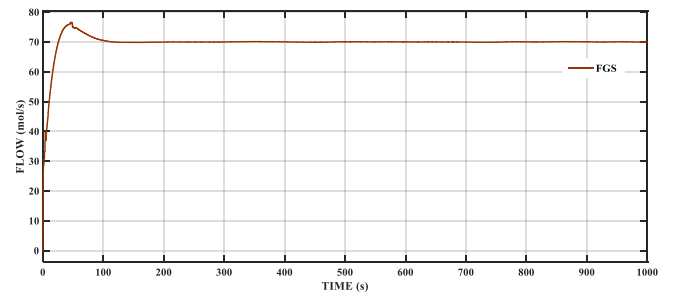


Fig.9. Flow performance of FGS-based parallel cascade control at 70mols/s

From the figure 9, it is noted that peak overshoot is reduced compare to PID control. Meanwhile settling time is also reduced.

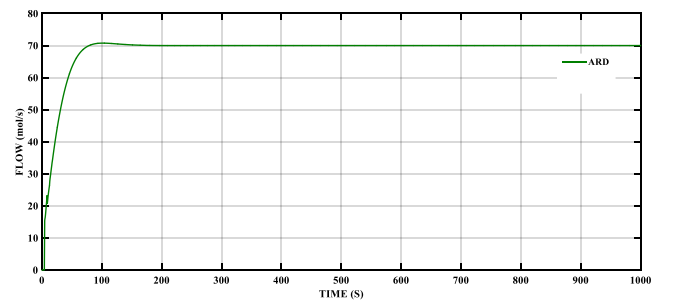


Fig.10. Flow performance of ARD algorithm based parallel cascade control at 70mols/s

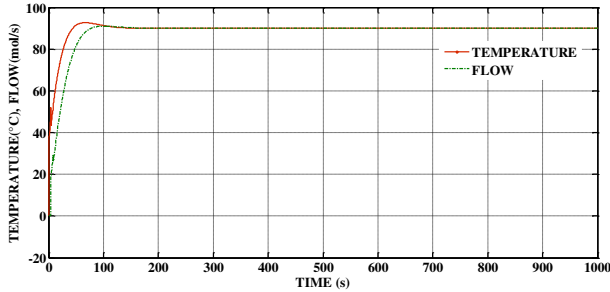


Fig.11. Performance of ARD algorithm based parallel cascade control at 90mol/s and 90°C

From the figure 11 it is noted that effect of ARD controller in outer loop reduces overshoot in flow compare to inner loop temperature. From this it is noted that overshoot produced inner loop is also reduced by outer loop ARD controller.

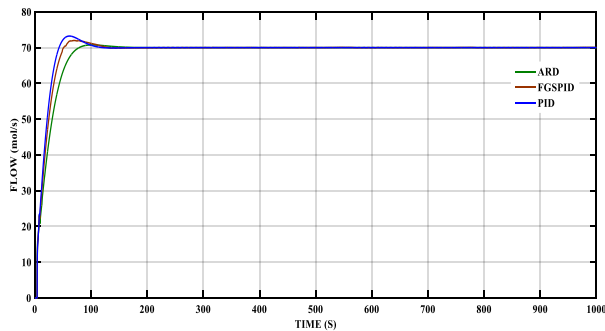


Fig.12. Comparative performance of Flow using parallel cascade control at 70mol/s

From the figure12, efficient performance of proposed system is noted that peak overshoot is effectively reduced compared to PID and FGS-PID controllers. Meantime steady state error is reduced compared to other controllers. The reduced peak overshoot and steady state error results in reduced ITAE compare to all other controllers as shown in Figure 13.

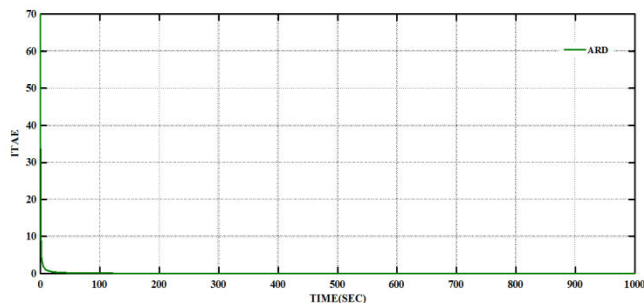


Fig.13. ITAE of ARD algorithm based parallel cascade control at 70mol/s

From the figure 13 it is noted that ITAE by ARD algorithm is very less due to effective control of flow. Comparative performance of all controllers in flow control at various flow levels are shown in figures 14 and 15.

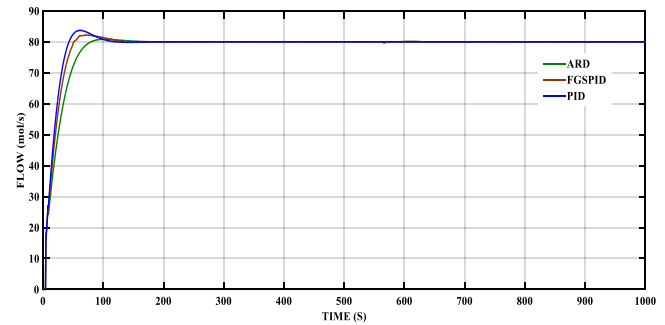


Fig.14. Comparative performance of Flow using parallel cascade control at 80mol/s

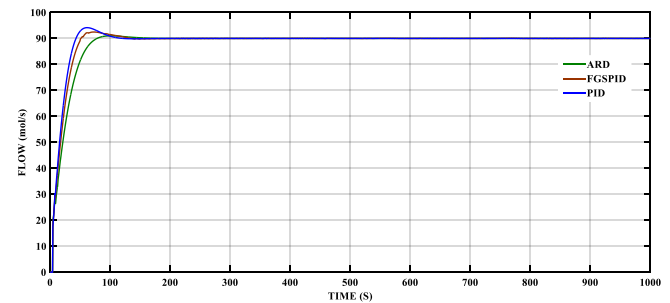


Fig.15. Comparative performance of Flow using parallel cascade control at 90 (mol/s)

From the figures 12,14 and 15 it is noted that at various flow levels ARD produces better performance than all other controllers. Comparative performance of PID based temperature control with various controllers in flow control is shown in figure 16.

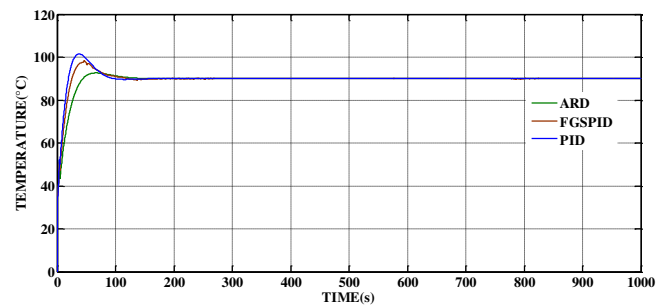


Fig.16. Comparative performance of Temperature using parallel cascade control at 90°C

From the figure 16 it is noted that inner loop controller in all cases are PID controller, but the effect of outerloop controller results various level of control on a temperature as shown in figure 16. FGS PID controller in an outer loop reduces temperature overshoot compare to PID in an outerloop. ARD as flow controller reduces overshoot in a temperature compare to all other controllers. From this analysis it is noted that ARD produces better performance in flow as well as in temperature control.

Table 4 Trade-off of various controllers in distillation at flow 70mols/s

Controller	Peak Overshoot (%)	Steady state error (%)	Rise time (sec)	Peak time (sec)	Settling time (sec)
PID	11.48	0.417	26.8	61.8	147
FGS	8.57	0.34	28.8	61.2	139
ARD	4.54	0.28	38.8	71.2	139

Table 5 Trade-off of various controllers in distillation at flow 80mols/s

Controller	Peak Overshoot (%)	Steady state error (%)	Rise time (sec)	Peak time (sec)	Settling time (sec)
PID	7	0.31	26.8	61.8	147
FGS	3.5	0.24	28.8	61.2	139
ARD	1	0.17	38.8	71.2	139

Table 6 Trade-off of various controllers in distillation at flow 90mols/s

Controller	Peak Overshoot (%)	Steady state error (%)	Rise time (sec)	Peak time (sec)	Settling time (sec)
PID	5.7	0.3	26.8	61.8	147
FGS	3.3	0.21	28.8	61.2	139
ARD	0.93	0.12	38.8	71.2	139

From the table 4, it is noted that compare to PID controller around 60% overshoot and 33% of steady state error are reduced by ARD algorithm.

From the tables4-6 it is noted that when flow increases, overshoot and steady state error are reduced. In all flow levels Peak overshoot and steady state are reduced by ARD algorithm compared to other controllers.

8. Conclusion

In this paper, a novel meta-heuristic method of artificial raindrop algorithm is proposed for control of flow with parallel cascade control of distillation column. Performance of proposed system is analyzed and compared with the performance of PID and FGS-PID based systems. FGS-PID controller reduces all parameters that were analysed when compare to PID based control. But from the analysis of FGS-PID, reduction in percentage of peak overshoot and steady state error is necessary. From the next set of analysis, it is noted that ARD algorithm control for flow produces better performance compared to PID and FGS-PID in aspects such as reduction in peak overshoot, peak time, rise time, settling time and steady state error. Peak overshoot and steady state error are reduced effectively by ARD algorithm which reduces the oscillation in flow and temperature of distillation column.

References

1. Biswas PP, Ray S, Samanta A.N.: *Nonlinear control of high purity distillation column under input saturation and parametric uncertainty*. In: Journal of Process Control, 2009, 19(1), pp.175-84
2. Bo, C., Li, J., Yang, L., Niu, C., Tang, J. Qiao, X.: *MPC of distillation column with side reactors for methylacetate*. In: Chinese Journal of Chemical Engineering, 2017
3. Cameron, C. Ruiz, R. Gani.: *A generalized model for distillation columns: Numerical and computational aspects*. In: Computers & chemical engineering, 1986, 10(3), pp.199-211
4. Chen Z, Henson MA, Belanger P, Megan L.: *Nonlinear model predictive control of high purity distillation columns for cryogenic air separation*. In: IEEE Transactions on Control Systems Technology, 2010, 18(4), pp.811-21
5. Cominos. P N. Munro.: *PID controllers: Recent tuning methods and design to specification*. In: IET Proceedings on Control Theory and Applications, 2002, 149(1), pp.46-53
6. Drgona. J, M. Klaučco, F. Janeček, M. Kvasnica.: *Optimal control of a laboratory binary distillation column via region less explicit MPC*. In: Computers & Chemical Engineering, 2017, pp.139-148
7. Gani. R, C. Ruiz, I. Cameron.: *A generalized model for distillation columns: Model description and applications*. In: Computers & chemical engineering, 1986, 10(3), pp.181-198
8. Gonzalez, I.O.B., Perez, R.R., Batlle, V.F., Fernandez, L.P.S. and Perez, L.A.S.: *Fuzzy Gain Scheduled Smith*

- Predictor for Temperature Control in an Industrial Steel Slab Reheating Furnace.* In: IEEE Latin America Transactions, 2016, 14(11), pp.4439-4447
9. Lee Y, Skliar M, Lee M.: *Analytical method of PID controller design for parallel cascade control.* In: Journal of Process Control, 2006, 16(8), pp.809-18
 10. Lee, Y.H., Oh, S., Park, S.: *Enhanced control with a general cascade control structure.* In: Industrial & Engineering Chemistry Research, 2002, 41(11), pp.2679–2688
 11. Luyben, W.L.: *Parallel cascade control.* In: Industrial and Engineering Chemistry Fundamentals, 1973, 12(4), pp.463-467
 12. Lutze P.: *Distillation in bio processing.* Distillation Operation and Applications, Gorak, A., Schoenmakers, H., Eds, 2014, pp.337-365
 13. Miccio M, Cosenza. B.: *Control of a distillation column by type-2 and type-1 fuzzy logic PID controllers.* In: Journal of Process Control, 2014, 24(5), pp.475–484
 14. Musch, H.E., Steiner, M.: *Robust PID control for an industrial distillation column.* In: IEEE Control Systems, 1995, 15(4), pp.46-55
 15. Puneet Mishra, Vineet Kumar, K.P.S. Rana.: *A fractional order fuzzy PID controller for binary distillation column control.* In: Expert Systems with Applications, 2015
 16. Padhan, D.G., Majhi S.: *Improved parallel cascade control structure for time delay processes.* In: India Conference, 2012, pp. 1-4
 17. Padhan, D.G., Majhi S.: *An improved parallel cascade control structure for processes with time delay.* In: Journal of Process Control, 2012, 22(5), pp.884-898
 18. Padhan D.G. Majhi S.: *Synthesis of PID tuning for a new parallel cascade control structure.* In: IFAC Proceedings Volumes, 2012, 45(3), pp.566-571
 19. Raja, G.L., Ali A.: *Modified parallel cascade control structure for integrating processes.* In: In Recent Developments in Control, Automation and Power Engineering (RDCAPE), International Conference on IEEE, 2015, pp. 90-95
 20. Santosh, S., Chidambaram, M.: *A simple method of tuning parallel cascade controllers for unstable FOPTD systems.* In: ISA transactions, 2016, (65), pp.475-486
 21. Savran, A., Kahraman G.: *A fuzzy model based adaptive PID controller design for nonlinear and uncertain processes.* In: ISA Transactions, 2014, (53), pp.280-288
 22. Semino, D., Brambilla, A.: *An efficient structure for parallel cascade control.* In: Industrial & Engineering Chemistry Research, 1996, (35), pp.1845–1852
 23. Sharma, R., Rana, P. S., Kumar, V.: *Performance analysis of fractional order fuzzy controller applied to robotic manipulator.* In: Expert Systems with Applications, 2014, 41(9), pp.4274 - 4289
 24. Skogestad. S.: *Dynamics and control of distillation columns A tutorial introduction.* In: Chemical Engineering Research and Design, 1997, 75(6), pp.539-562.
 25. Stenz, R., Kuhn, U.: *Automation of a batch distillation column using fuzzy and conventional control.* In: IEEE Transactions on Control Systems Technology, 1995, 3(2), pp.171-176
 26. Tschanz, F., Zentner, S., Onder, C.H. and Guzzella, L.: *Cascaded control of combustion and pollutant emissions in diesel engines.* In: Control Engineering Practice, 2014, (29), pp.176-186
 27. Wang, L.: *Automatic tuning of PID controllers using frequency sampling filters.* In: IET Control Theory and Applications, 2017, 11(7), pp.985-995
 28. Yamamoto. T, S. Shah.: *Design and experimental evaluation of a multivariable self-tuning PID controller.* In: IET Proceedings on Control Theory and Applications, 2004, 151(5), pp.645–652
 29. Yahia, R.A.A. Boucherit, M.S.: *Fuzzy Control of a Distillation Column.* In: WSEAS transactions on systems, (7), pp.2476-2480
 30. Zadeh, L. A.: *Fuzzy sets.* In: Information and Control, 1965, 8(3), pp.338–353
 31. Zhao Z.Y, M. Tomizuka, S. Isaka.: *Fuzzy gain scheduling of PID controllers.* In: IEEE Transactions on Systems, Man and Cybernetics, 1993, 23(5), pp.1392-1398